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(54) Title: PROCESS FOR PRODUCING CRYSTALLINE 1,2-POLYBUTADIENE

(54) 発明の名称: 結晶性 1, 2-ポリブタジエンの製造方法

(57) **Abstract:** 1,3-Butadiene is polymerized in a hydrocarbon solvent using either a catalyst system comprising (A) a cobalt salt, (B1) a phosphine compound having one C₃ or higher branched aliphatic group or C₅ or higher alicyclic group and two aromatic groups, and (C) an organoaluminum compound or a catalyst system comprising (A) a cobalt salt, (B) at least one of (B1) a phosphine compound having one C₃ or higher branched aliphatic group or C₅ or higher alicyclic group and two aromatic groups and (B2) a triarylphosphine compound having three aromatic groups, (C) an organoaluminum compound, and (D) an active halogen to obtain crystalline 1,2-polybutadiene.

(57) 要約: (A) コバルト塩、(B1) 炭素数 3 以上の分岐を有する脂肪族基または炭素数 5 以上の脂環族基を 1 つと芳香族基を 2 つ有するホスフィン化合物、および (C) 有機アルミニウム化合物を含む触媒系、あるいは、(A) コバルト塩、(B) (B1) 炭素数 3 以上の分岐を有する脂肪族基もしくは炭素数 5 以上の脂環族基を 1 つと芳香族基を 2 つ有するホスフィン化合物および/または (B2) 芳香族基を 3 つ有するトリアリールホスフィン化合物、(C) 有機アルミニウム化合物、ならびに (D) 活性ハロゲンを含む触媒系を使用して、1, 3-ブタジエンを、炭化水素溶媒中で重合し、結晶性 1, 2-ポリブタジエンを得る。

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Description

Process for Producing Crystalline 1,2-Polybutadiene

5 Technical Field

The present invention relates to a process for producing crystalline 1,2-polybutadiene, and more particularly to a process for producing 1,2-polybutadiene having a high crystallinity using a specific catalyst system, wherein the
10 vinyl bond content of a polymer obtained is high, and the molecular weight thereof is adjustable.

Background Art

1,2-Polybutadiene having crystallinity has hitherto been
15 obtained by a catalyst comprising a phosphine complex of a cobalt salt, a trialkylaluminum and water (patent document 1: JP-B-44-32425, patent document 2: JP-A-1-249788), a catalyst comprising a phosphine complex of a cobalt salt and methylaluminoxane (patent document 3: JP-A-8-59733), or a
20 catalyst comprising a cobalt salt slurry, a phosphine solution and methylaluminoxane [non-patent document 1: Dilip C. D. Nath, Takeshi Shiono and Tomiki Ikeda, *Journal of Polymer Science*, Vol. 40, 3086-3092 (2002)].

In the catalyst systems described these, it can be known
25 by analogy that a phosphine compound having three aromatic groups is substantially necessary in the production of a 1,2-polybutadiene-based polymer having a crystallinity of 34%

or more. However, when those phosphine compounds are used, it is required to lower the polymerization temperature, which causes an increase in the amount of a solvent used for preventing precipitation, and in the production of the 1,2-poly-
5 butadiene-based polymer obtained by an exothermic reaction, the problem of increasing energy loss such as the necessity for higher cooling capacity to a polymerization reactor.

In the above-mentioned patent document 1 (JP-B4432425), there is described an example to use diphenylethylphosphine as
10 a phosphine compound having one aliphatic group and two aromatic groups. However, it is described that an amorphous (that is to say, having a crystallinity of 0%) polymer is obtained when the phosphine compound is used. It is difficult to know the production of a 1,2-polybutadiene-based polymer having a
15 crystallinity of 34% or more by analogy with the category of phosphines as specifically exemplified in the gazette concerned, that is to say, the phosphine compound having one aliphatic group and two aromatic groups.

Further, in the catalyst systems described in these, when
20 the phosphine complex of the cobalt salt is used, equipment for preparing a catalyst component becomes large to necessitate excessive investment, because of low solubility of the phosphine complex in an organic solvent. Furthermore, when a cobalt chloride slurry is used, the efficiency of catalyst is
25 low. It is therefore necessary to use a large amount of catalyst in order to obtain a polymer, which causes the problems of the coloration of the polymer due to residual catalyst and the like.

The present invention relates to a process for producing 1,2-polybutadiene having a high crystallinity using a specific catalyst system, wherein the vinyl bond content of a polymer obtained is high, and the molecular weight thereof is
5 adjustable.

Disclosure of the Invention

The present invention relates to a process for producing crystalline 1,2-polybutadiene, which is characterized in that
10 1,3-butadiene is polymerized in a hydrocarbon solvent using a catalyst system comprising (A) a cobalt salt, (B1) a phosphine compound having one branched aliphatic group of 3 or more carbon atoms or one alicyclic group of 5 or more carbon atoms and two aromatic groups, and (C) an organic aluminum compound
15 (hereinafter also referred to as "production process 1").

Brief Description of the Drawing

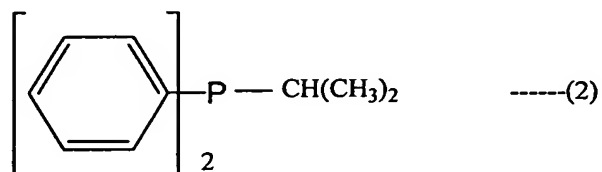
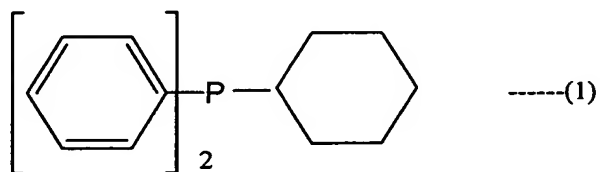
Fig. 1 is a flow chart showing a preferred production process for obtaining crystalline 1,2-polybutadiene of the
20 present invention.

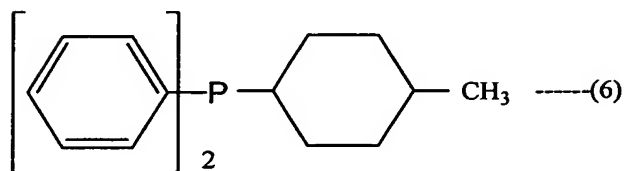
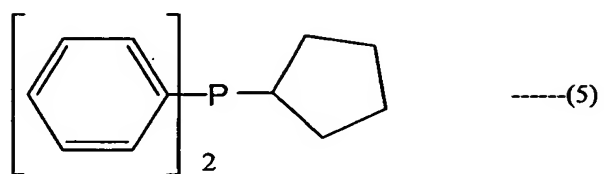
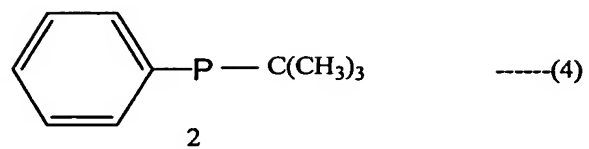
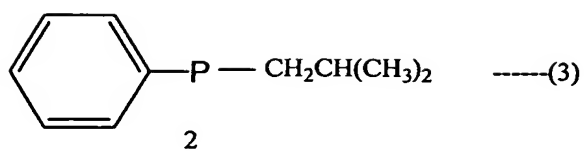
Best Mode for Carrying Out the Invention

(A) The cobalt salt used in the catalyst of the present invention is a cobalt salt of an organic acid such as cobalt
25 chloride, cobalt bromide, cobalt iodide, cobalt octylate, cobalt versatate or cobalt naphthenate, or the like, and a cobalt salt of an organic acid such as cobalt octylate, cobalt

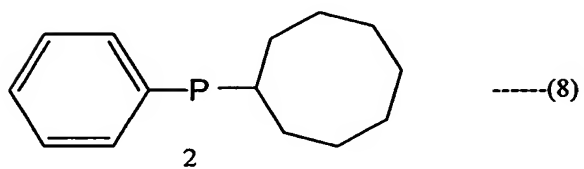
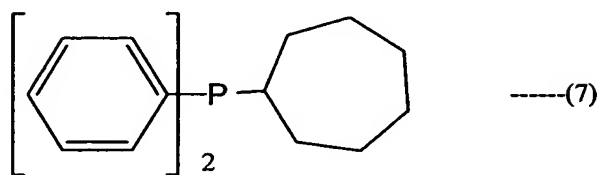
versatate or cobalt naphthenate is preferred in that no halogen atom is contained. Further, of these, cobalt octylate, cobalt versatate or cobalt naphthenate is preferred from the point of high solubility in an organic solvent.

5 Further, as (B1) the above-mentioned phosphine compound having one branched aliphatic group of 3 or more carbon atoms or one alicyclic group of 5 or more carbon atoms and two aromatic groups, there is preferably used, for example, a phosphine compound having one branched aliphatic group of 3 or more carbon
 10 atoms or one alicyclic group of 5 or more carbon atoms and two aromatic groups such as phenyl groups, such as diphenylcyclohexylphosphine shown in formula (1), diphenylisopropylphosphine shown in formula (2), diphenylisobutylphosphine shown in formula (3), diphenyl-t-butylphosphine
 15 shown in formula (4), diphenylcyclopentylphosphine shown in formula (5), diphenyl(4-methylcyclohexyl)phosphine shown in formula (6), diphenylcycloheptylphosphine shown in formula (7) or diphenylcyclooctylphosphine shown in formula (8).





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When this catalyst system comprising (A) the cobalt salt, (B1) the phosphine compound having one branched aliphatic group of 3 or more carbon atoms or one alicyclic group of 5 or more carbon atoms and two aromatic groups and (C) the organic aluminum compound is used, a mixed system of (A) to (C) may be used. However, it is preferred that component (C) is used in combination with a phosphine complex of a cobalt salt comprising component (A) and component (B1). When the phosphine complex of the cobalt salt comprising component (A) and component (B1) is used, there may be used either one previously synthesized, or a method of bringing (A) the cobalt salt into contact with (B1) the phosphine compound having one branched aliphatic group of 3 or more carbon atoms or one alicyclic group of 5 or more carbon atoms and two aromatic groups, in a polymerization system.

Specific examples of the phosphine complexes of the cobalt salts comprising (A) the cobalt salt and (B1) the phosphine compound having one branched aliphatic group of 3 or more carbon atoms or one alicyclic group of 5 or more carbon atoms and two aromatic groups include cobaltbis(diphenylcyclohexylphosphine) dichloride, cobaltbis(diphenylcyclohexylphosphine) dibromide, cobaltbis(diphenylisopropylphosphine) dichloride, cobaltbis(diphenylisopropylphosphine) dibromide, cobaltbis(diphenylisobutylphosphine) dichloride, cobaltbis(diphenylisobutylphosphine) dibromide, cobaltbis(diphenyl-t-butylphosphine) dichloride, cobaltbis(diphenyl-t-butylphosphine) dibromide and the like, and preferred

are cobaltbis(diphenylcyclohexylphosphine) dichloride and cobaltbis(diphenylcyclohexylphosphine) dibromide.

Further, (C) the organic aluminum compounds include methylaluminoxane or a compound obtained by bringing a
5 trialkylaluminum into contact with water.

Of these, as methylaluminoxane, there may be used either one previously synthesized or one synthesized in the polymerization system.

Besides, the above-mentioned trialkylaluminum is
10 trimethylaluminum, triethylaluminum, triisobutylaluminum, trioctylaluminum or the like, and water is used in an amount of 0.2 to 1.0, preferably 0.3 to 0.75, by the molar ratio based on the aluminum atom of the trialkylaluminum.

As for a contacting method of the trialkylaluminum and
15 water, water may be brought into contact with an inert organic solvent solution of the trialkylaluminum, in any state of vapor, liquid and solid (ice). Further, water may be brought into contact, as a dissolved state, a dispersed state or an emulsified state in an inert organic solvent, or as a gas state
20 or a mist state where it exists in an inert gas.

In the catalyst used in production process 1 of the present invention, the use ratio of (A) the cobalt salt and (B1) the phosphine compound is preferably 1 to 5 mol of (B1) the phosphine compound per mol of (A) the cobalt salt.

25 Further, the amount of the phosphine complex of the cobalt salt comprising components (A) and (B1) used is within the range of 5,000 to 150,000, preferably 10,000 to 100,000, by the molar

ratio of 1,3-butadiene and the cobalt atom in the phosphine complex (1,3-butadiene/Co). When 1,3-butadiene/Co (molar ratio) is less than 5,000, the mechanical strength of a polymer obtained is inferior. On the other hand, exceeding 150,000 results in decreased polymerization activity.

Furthermore, the amount of component (C) (organic aluminum compound) used is within the range of 500 to 4,000, preferably 800 to 2,000, by the molar ratio of 1,3-butadiene and the aluminum atom in component (C) (1,3-butadiene/Al). When 1,3-butadiene/Al (molar ratio) is less than 500, it is economically disadvantageous. On the other hand, exceeding 4,000 results in decreased polymerization activity. The ratio of the aluminum atom of component (C) to the cobalt atom of the phosphine complex of the cobalt salt comprising components (A) and (B1) (Al/Co) is usually from 5 to 300, and preferably about 7.5 to 100. When Al/Co (atomic ratio) is less than 5, polymerization activity is decreased. On the other hand, exceeding 300 results in economical disadvantage.

The catalyst used in production process 1 of the present invention is prepared by mixing catalyst components in an inert organic solvent in any order. Preferably, as shown in Fig. 1, (A) the cobalt salt is allowed to react with (B1) the phosphine compound in an inert organic solvent to form the phosphine complex of the cobalt salt, then, component (C) is added thereto to prepare the catalyst of the present invention, and 1,3-butadiene is polymerized in a hydrocarbon solvent using this catalyst, thereby obtaining crystalline 1,2-poly-

butadiene.

Further, the amount of (A) the cobalt salt used is within the range of 5,000 to 200,000, preferably 10,000 to 150,000, by the molar ratio of the 1,3-diene and the cobalt atom (1,3-diene/Co). When 1,3-diene/Co (molar ratio) is less than 5,000, the mechanical strength of a polymer obtained is inferior. On the other hand, exceeding 200,000 results in decreased polymerization activity.

Furthermore, the amount of component (C) (aluminoxane) used is within the range of 500 to 4,000, preferably 1000 to 3,000, by the molar ratio of the 1,3-diene and the aluminum atom in component (C) (1,3-diene/Al). When 1,3-diene/Al (molar ratio) is less than 500, it is economically disadvantageous. On the other hand, exceeding 4,000 results in decreased polymerization activity. The ratio of the aluminum atom of component (C) to the cobalt atom of component (A) (Al/Co) is usually from 5 to 300, and preferably from about 7.5 to 100. When Al/Co (atomic ratio) is less than 5, polymerization activity is decreased. On the other hand, exceeding 300 results in economical disadvantage.

As the inert organic solvents used for the preparation of the catalysts in the above-mentioned production processes 1 and 2 of the present invention, there can be used, for example, an aromatic hydrocarbon such as benzene, toluene or xylene, an aliphatic hydrocarbon such as butane, butene, pentane, pentene, hexane, heptane or octane, an alicyclic hydrocarbon such as cyclopentane or cyclohexane, a chlorinated hydrocarbon such as

methylen chloride, 1,2-dichloroethane, 1,1,1-trichloroethane, chlorobenzene, o-dichlorobenzene or p-dichlorobenzene, and a mixture thereof.

As the inert organic solvents used for the preparation of the catalysts, there are also preferably used the same solvents as the polymerization catalysts.

Further, the catalyst may be prepared by previously mixing respective components before it is brought into contact with 1,3-butadiene of the present invention, or can also be prepared by mixing respective components in the presence of a conjugated diene in a polymerization reactor.

In the present invention, 1,2-polybutadiene having a crystallinity of 5% to 40% can be produced by polymerizing 1,3-butadiene in the hydrocarbon solvent using the catalyst system mainly comprising components (A), (B1) and (C).

In the present invention, a conjugated diene other than 1,3-butadiene can also be used together in an amount of about 10% by weight or less. The conjugated dienes other than 1,3-butadiene, which are used in the present invention, include a 4-alkyl-substituted-1,3-butadiene, a 2-alkyl-substituted-1,3-butadiene and the like. Of these, the 4-alkyl-substituted-1,3-butadienes include 1,3-pentadiene, 1,3-hexadiene, 1,3-heptadiene, 1,3-octadiene, 1,3-nonadiene, 1,3-decadiene and the like. Further, typical examples of the 2-alkyl-substituted-1,3-butadienes include 2-methyl-1,3-butadiene (isoprene), 2-ethyl-1,3-butadiene, 2-propyl-1,3-butadiene, 2-isopropyl-1,3-butadiene, 2-butyl-1,3-butadiene,

2-isobutyl-1,3-butadiene, 2-amyl-1,3-butadiene, 2-isoamyl-1,3-butadiene, 2-hexyl-1,3-butadiene, 2-cyclohexyl-1,3-butadiene, 2-isoheptyl-1,3-butadiene, 2-heptyl-1,3-butadiene, 2-isoheptyl-1,3-butadiene, 2-octyl-1,3-butadiene, 2-iso-octyl-1,3-butadiene and the like. Of these conjugated dienes, preferred examples of the conjugated dienes used as a mixture with 1,3-butadiene include isoprene and 1,3-pentadiene.

The hydrocarbon solvents used as the polymerization solvents include, for example, an aromatic hydrocarbon such as benzene; toluene or xylene, an aliphatic hydrocarbon such as butane, butene, pentane, pentene, hexane, heptane or octane, an alicyclic hydrocarbon such as cyclopentane or cyclohexane, a chlorinated hydrocarbon such as methylene chloride, 1,2-dichloroethane, 1,1,1-trichloroethane, chlorobenzene, o-dichlorobenzene or p-dichlorobenzene, and a mixture thereof. Preferred examples thereof include cyclohexane, heptane, toluene, methylene chloride and the like. More preferred is a non-halogen hydrocarbon solvent such as cyclohexane, heptane or toluene, from the standpoint of the non-halogen series.

The polymerization temperature is usually from -20°C to $+120^{\circ}\text{C}$, and preferably from $+10^{\circ}\text{C}$ to $+90^{\circ}\text{C}$. The polymerization reaction may be conducted by either a batch system or a continuous system. The monomer concentration in the solvent is usually from 5 to 80% by weight, and preferably from 8 to 40% by weight.

Further, in order to produce a polymer, it is necessary that attention is taken to avoid contamination with a compound

having inactivating action, such as oxygen, water or carbon dioxide, to the utmost in the polymerization system for preventing inactivation of the catalyst and the polymer of the present invention.

5 When the polymerization reaction has proceeded to a desired stage, a polymerization terminator such as an alcohol, an antioxidant, an antiaging agent, an ultraviolet ray absorber and the like are added to a reaction mixture, and then, a polymer formed according to an usual method is separated, washed and
10 dried to be able to obtain desired 1,2-polybutadiene.

1,2-Polybutadiene obtained by the production process of the present invention has a vinyl bond content of 85% or more, preferably 90% or more.

Further, the crystallinity of 1,2-polybutadiene obtained
15 by the present invention is preferably from 5 to 40%, and more preferably from 10 to 35%. Less than 5% results in inferior mechanical strength, whereas exceeding 40% results in inferior processability. The crystallinity is adjustable by the polymerization temperature or the like.

20 Furthermore, the molecular weight of 1,2-polybutadiene obtained by the present invention is usually from 100,000 to 600,000, by the weight average molecular weight in terms of polystyrene. Less than 100,000 results in inferior strength, whereas exceeding 600,000 results in inferior processability.
25 The molecular weight is adjustable by the aluminum atom/cobalt atom ratio.

The halogen atom content in 1,2-polybutadiene of the

present invention thus obtained is preferably low from the standpoint of environmental problems, and is 200 ppm or less, more preferably 100 ppm or less and particularly preferably 50 ppm or less. Exceeding 200 ppm results in an increase in the amount of endocrine disrupter corresponding materials generated in burning in some cases.

Here, the halogen atom content of the resulting polymer can be easily adjusted to 200 ppm or less by using a non-halogen cobalt salt in the catalyst system, particularly in component (B1) or component (B), and by using the above-mentioned non-halogen hydrocarbon solvent as the solvent for catalyst preparation or the polymerization solvent.

Crystalline 1,2-polybutadiene obtained by the present invention is blended as a raw resin or raw rubber, either alone or as a mixture with another synthetic resin, synthetic rubber or natural rubber, further, oil extended with a process oil as needed, and then, ordinary compounding agents for vulcanized rubber such as a filler such as carbon black, a vulcanizing agent and a vulcanization accelerator are added to perform vulcanization as a rubber composition, thereby being able to use for applications requiring mechanical characteristics and wear resistance, for example, tires, hoses, belts, sponges, footwear materials, sheets, films, tubes, packaging materials, resin modifiers, photosensitive materials and other various industrial goods.

Examples

The present invention will be illustrated in greater detail with reference to the following examples, but the invention should not be construed as being limited by the following examples, as long as it does not exceed a gist thereof.

5 In the examples, parts and percentages are on a weight basis, unless otherwise specified.

Further, various measurements in the examples were made in accordance with the following methods.

7 The vinyl bond content (1,2-bond content) of
10 1,2-polybutadiene was determined by an infrared absorption spectrum method (the Morero's method).

 The crystallinity of 1,2-polybutadiene was converted from the density measured by an underwater substitution method, taking the density of 1,2-polybutadiene at a crystallinity of
15 0% as 0.889 g/cm³, and the density of 1,2-polybutadiene at a crystallinity of 100% as 0.963 g/cm³.

 The weight average molecular weight (Mw) was measured by gel permeation chromatography (GPC) at 40°C using tetrahydrofuran as a solvent.

20 The halogen atom content was determined by a fluorescent X-ray measurement (FP method).

 The melt flow index (MI) showed the amount (g) of a resin flowed out for a period of time corresponding to 10 minutes under conditions of a temperature of 150 °C and a load of 2.16 kilograms,
25 with a melt flow indexer.

Example 1

Preparation of Cobaltbis(diphenylcyclohexylphosphine)

Dichloride Solution:

In an atmosphere of dry nitrogen, 2.2 g of anhydrous cobalt chloride, 8.0 g of diphenylcyclohexylphosphine and 125 g of methylene chloride were added into a 300-ml pressure bottle, and stirred in a constant temperature water bath of 35°C for 4 hours, followed by separation of a precipitate to obtain an 8% methylene chloride solution of cobaltbis(diphenylcyclohexylphosphine) dichloride. This solution was diluted with methylene chloride, and used as a 0.4% solution.

Polymerization of 1,3-Butadiene:

In an atmosphere of dry nitrogen, 25 g of 1,3-butadiene (BD) and 125 g of cyclohexane were put into a 300-ml pressure bottle, and the 0.4% solution of cobaltbis(diphenylcyclohexylphosphine) dichloride obtained above and a 1% (as Al atoms) solution of methylaluminoxane in toluene were each added so as to give BD/Co (molar ratio) = 30,000 and Al/Co (atomic ratio) = 20, respectively, followed by polymerization in a constant temperature water bath of 50°C for 120 minutes.

Reaction termination was performed by adding a small amount of ethanol as a terminator.

Then, 2,6-di-t-butyl-p-cresol was added in an amount of 0.3 part based on 100 parts of the polymer, and heated on a hot plate to remove the solvents, thereby obtaining the polymer. The degree of polymerization conversion was determined from the yield. Further, the halogen content in the polymer was measured. The results are shown in Table 1.

Examples 2 to 7

Using the same technique as with Example 1, by cobalt salts and phosphine compounds shown in Table 1, solutions of phosphine complexes of the cobalt salts were prepared, and polymerization of 1,3-butadiene was conducted under conditions of BD/Co ratios and Al/Co ratios shown in Table 1. The results are shown in Table 1.

Comparative Examples 1 to 4

Using the same technique as with Example 1, by cobalt salts and phosphine compounds shown in Table 1, solutions of phosphine complexes of the cobalt salts were prepared, and polymerization of 1,3-butadiene was conducted under conditions of BD/Co ratios and Al/Co ratios shown in Table 1. The results are shown in Table 2.

Table 1

	Example 1	Example 2	Example 3	Example 4	Example 5	Example 6	Example 7
Polymerization Solvent	Cyclohexane	Cyclohexane	Cyclohexane	Cyclohexane	Cyclohexane	Cyclohexane	Cyclohexane
Solvent/1,3-Butadiene (Weight Ratio)	5	5	5	5	5	5	5
Cobalt Salt	Cobalt Chloride	Cobalt Chloride	Cobalt Chloride	Cobalt Bromide	Cobalt Chloride	Cobalt Chloride	Cobalt Chloride
Phosphine Compound	Diphenyl cyclohexylphosphine	Diphenyl cyclohexylphosphine	Diphenyl cyclohexylphosphine	Diphenyl cyclohexylphosphine	Diphenyl isopropylphosphine	Diphenyl isobutylphosphine	Diphenyl t-butylphosphine
Polymerization Temperature	50°C	50°C	50°C	50°C	50°C	50°C	50°C
Polymerization Time	120 min	120 min	120 min	120 min	120 min	120 min	120 min
BD/Co (Molar Ratio)	30,000	45,000	60,000	90,000	45,000	60,000	60,000
Al/Co (Atomic Ratio)	20	30	40	60	30	40	40
Degree of Polymerization Conversion	82%	80%	80%	81%	81%	82%	78%
State of Solution	Uniform	Uniform	Uniform	Uniform	Uniform	Uniform	Uniform
Vinyl Bond Content	95%	95%	95%	94%	94%	91%	92%
Crystallinity	37%	37%	37%	36%	36%	34%	34%
Weight Average Molecular Weight	150,000	170,000	230,000	140,000	160,000	180,000	170,000
Halogen Content	45 ppm	36 ppm	27 ppm	40 ppm	35 ppm	28 ppm	30 ppm

Table 2

	Compara- tive Example 1	Compara- tive Example 2	Compara- tive Example 3	Compara- tive Example 4
Polymerization Solvent	Cyclo-hexane	Cyclo-hexane	Cyclo-hexane	Cyclo-hexane
Solvent/1,3-Butadiene (Weight Ratio)	5	5	5	5
Cobalt Salt	Cobalt Chloride	Cobalt Chloride	Cobalt Bromide	Cobalt Bromide
Phosphine Compound	Tris(3,5-dimethyl-phenyl)-phosphine	Tris(3,5-dimethyl-phenyl)-phosphine	Tris(3,5-dimethyl-phenyl)-phosphine	Tris(3,5-dimethyl-phenyl)-phosphine
Polymerization Temperature	50°C	30°C	50°C	30°C
Polymerization Time	120 min	180 min	120 min	180 min
BD/Co (Molar Ratio)	60,000	60,000	90,000	90,000
Al/Co (Atomic Ratio)	40	40	60	60
Degree of Polymerization Conversion	80%	78%	81%	79%
State of Solution	Uniform	Precipitated	Uniform	Precipitated
Vinyl Bond Content	92%	94%	92%	94%
Crystallinity	25%	35%	24%	35%
Weight Average Molecular Weight	190,000	220,000	210,000	250,000
Halogen Content	28 ppm	28 ppm	39 ppm	42 ppm

As apparent from Tables 1 and 2, it turns out that the polymers having a high crystallinity can be obtained at a polymerization temperature of 50°C in Examples 1 to 7, but that the polymerization temperature must be lowered to 30°C in Comparative Examples 1 to 4, in order to obtain an equivalent crystallinity. Consequently, Examples 1 to 7 require a shorter polymerization time, but Comparative Examples 2 and 4 require a longer polymerization time, which practically causes a problem.

Example 8

Preparation of Phosphine Complex Solution:

Using the same technique as with Example 1, by a cobalt salt and a phosphine compound shown in Table 3, a solution of a phosphine complex of the cobalt salt was prepared.

Polymerization of 1,3-Butadiene:

In an atmosphere of dry nitrogen, 25 g of 1,3-butadiene (BD) and 250 g of methylene chloride were put into a 300-ml pressure bottle, and water in the system was adjusted to water/Al (molar ratio) = 0.7. In a state cooled to 10°C, an 8% solution of triisobutylaluminum in methylene chloride was added so as to give BD/Co (molar ratio) = 20,000 and Al/Co (atomic ratio) = 20, followed by thorough stirring. Then, the resulting solution of the phosphine complex of the cobalt salt was added so as to give BD/Co (molar ratio) = 20,000, and thereafter, the bottle was immediately placed in a constant temperature water bath of 20°C, followed by polymerization for 60 minutes.

Reaction termination was performed by adding a small amount of ethanol as a terminator. Then, 2,6-di-t-butyl-p-cresol was added in an amount of 0.3 part based on 100 parts of the polymer, and heated on a hot plate to remove the solvents, thereby obtaining the polymer. The degree of polymerization conversion was determined from the yield. The results are shown in Table 3.

Comparative Examples 5 to 7

Using the same technique as with Example 8, by cobalt salts and phosphine compounds shown in Table 2, solutions of phosphine complexes of the cobalt salts were prepared, and polymerization of 1,3-butadiene was conducted under conditions of BD/Co ratios and Al/Co ratios shown in Table 3. The results are shown in Table 3.

Table 3

	Example 8	Comparative Example 5	Comparative Example 6	Comparative Example 7
Polymerization Solvent	Methylene Chloride	Methylene Chloride	Methylene Chloride	Methylene Chloride
Solvent/1,3-Butadiene (Weight Ratio)	10	10	10	10
Cobalt Salt	Cobalt Bromide	Cobalt Bromide	Cobalt Bromide	Cobalt Bromide
Phosphine Compound	Diphenyl-cyclohexyl phosphine	Tris(3,5-dimethyl-phenyl)-phosphine	Tris(3,5-dimethyl-phenyl)-phosphine	Tris(3,5-dimethyl-phenyl)-phosphine
Polymerization Temperature	20°C	20°C	-5°C	20°C
Polymerization Time	60 min	60 min	90 min	60 min
BD/Co (Molar Ratio)	20,000	20,000	15,000	20,000
Al/Co (Atomic Ratio)	20	20	15	20
Degree of Polymerization Conversion	86%	81%	83%	84%
State of Solution	Uniform	Uniform	Precipitated	Uniform
Vinyl Bond Content	95%	92%	95%	93%
Crystallinity	38%	29%	37%	30%
Weight Average Molecular Weight	160,000	170,000	180,000	160,000
Halogen Content	351 ppm	387 ppm	524 ppm	483 ppm

As apparent from Table 3, it turns out that the polymer having a high crystallinity has been obtained at a polymerization temperature of 20°C in Example 8,

but that the polymers having a low crystallinity have been obtained at a polymerization temperature of 20°C in Comparative Examples 5 and 7. On the other hand, it turns out that the polymerization temperature must be lowered to -5°C in Comparative Example 6, in order to obtain an equivalent crystallinity. Consequently, Example 8 requires a shorter polymerization time, but Comparative Example 6 requires a longer polymerization time, which practically causes a problem.

As described above, in a method which can be known by analogy from the descriptions of JP-B-44-32425, JP-A-1-249788 and JP-A-8-59733, that is to say, in a case that a phosphine compound having three aromatic groups is used as the phosphine compound, a lower crystallinity is obtained under equivalent conditions. When it is intended to obtain a polymer having an equivalent crystallinity, the polymerization temperature must be lowered, which causes an increase in the amount of a solvent used for preventing precipitation, and in the production of the 1,2-polybutadiene obtained by an exothermic reaction, the problem of increasing energy loss such as the necessity for higher cooling capacity to a polymerization reactor. It is therefore apparent that the method is industrially disadvantageous.

Industrial Applicability

Crystalline 1,2-polybutadiene obtained by the present invention is blended as a raw resin or raw rubber, either alone or as a mixture with another synthetic resin,

synthetic rubber or natural rubber, further, oil extended with a process oil as needed, and then, ordinary compounding agents for vulcanized rubber such as a filler such as carbon black, a vulcanizing agent and a vulcanization accelerator are added to perform vulcanization as a rubber composition, thereby being able to use for applications requiring mechanical characteristics and wear resistance, for example, tires, hoses, belts, sponges, footwear materials, sheets, films, tubes, packaging materials, resin modifiers, photosensitive materials and other various industrial goods.